

Equilibrio inicial:

P. 1.3

$$T_{AO} = \frac{P_{AO} V_0}{n_A R} \quad P_{AO} = P_{BO} \quad (\text{Equilibrio del sistema adiabático})$$

$$T_{BO} = T_0 = \frac{P_{BO} V_0}{n_B R} \quad P_{BO} = \frac{n_B R T_0}{V_0}$$

$$P_{BO} = P_{AO} = \frac{T_{AO} n_A R}{V_0} = \frac{n_B R T_0}{V_0}$$

$$T_{AO} = T_0 \frac{n_B}{n_A}$$

Compresión adiabática del gas en A:

$$T_{Af} V_{Af}^{(r-1)} = T_{AO} V_0^{(r-1)} \quad T_{Af} \left(\frac{V_0}{2}\right)^{(r-1)} = T_{AO} V_0^{(r-1)}$$

$$T_{Af} = T_{AO} 2^{(r-1)} = T_0 \frac{n_B}{n_A} 2^{(r-1)}$$

para las presiones en la compresión adiabática

$$P_{Af} V_{Af}^r = P_{AO} V_0^r \quad P_{Af} \left(\frac{V_0}{2}\right)^r = P_{AO} V_0^r$$

$$P_{Af} = P_{AO} 2^r = \frac{n_A R T_{AO}}{V_0} 2^r = \frac{n_A R T_0}{V_0} \frac{n_B}{n_A} 2^r$$

$$P_{Af} = \frac{n_A R T_{AO}}{V_0} 2^r = \frac{n_B R T_0}{V_0} 2^r$$

$P_{AO} = P_{BO}$

$$\text{El volumen } V_{Bf} = \frac{n_B RT_0}{P_{Bf}} \quad P_{Bf} = P_{Af}$$

$$V_{Bf} = \frac{n_B RT_0}{P_{Bo} 2^r} = \left(\frac{\frac{n_B RT_0}{P_{Bo}}}{2^r} \right) V_o = V_o 2^{-r}$$

Para el gas en A $Q_A = 0 \quad \Delta U_A = W_A$

$$W_A = \frac{n_A R}{r-1} (T_{Af} - T_{Ao}) = \frac{n_A R}{r-1} \left(T_0 \frac{n_B}{n_A} 2^{(r-1)} - T_0 \frac{n_B}{n_A} \right)$$

$$W_A = \frac{n_B R}{r-1} T_0 (2^{(r-1)} - 1)$$

El calor intercambiado por el gas en B con el fondo es $\Delta U_B = 0 = Q_B + W_B \quad Q_B = -W_B$

$$Q_B = \int_{V_o}^{V_{Bf}} P \, dv = \int_{V_o}^{V_{Bf}} \frac{n_B RT_0}{V} \, dv$$

$$Q_B = n_B RT_0 \ln \left(\frac{V_{Bf}}{V_o} \right) = n_B RT_0 \ln \left(\frac{V_o 2^{-r}}{V_o} \right)$$

$$Q_B = -n_B RT_0 r \ln 2 < 0$$

